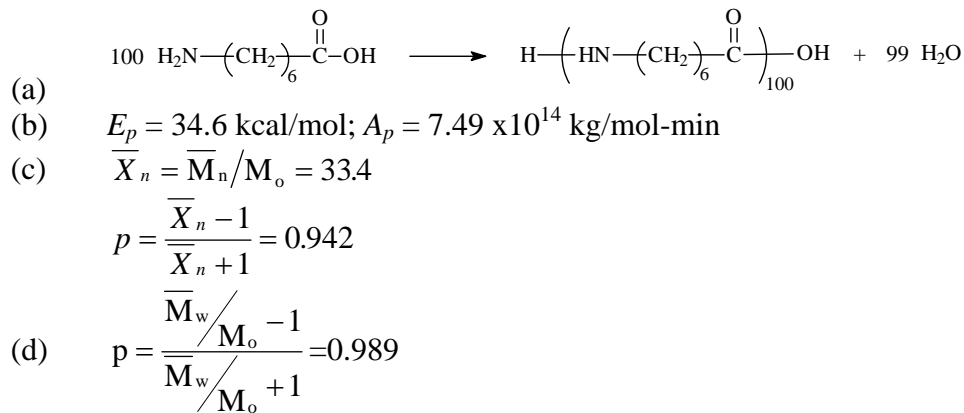


1. (a) $\bar{M}_n = 57,143 \text{ g/mol}$
 (b) $\bar{M}_w = 83,333 \text{ g/mol}$

2. (a) $\bar{M}_n = 108,538 \text{ g/mol}$
 (b) $\bar{M}_w = 137,358 \text{ g/mol}$
 (Each fraction was assigned the mid-point molecular weight.)

3. $M_o = 100 \text{ g/mol}$
 (a) $p = \frac{\bar{M}_w/M_o - 1}{\bar{M}_w/M_o + 1} = 0.989$
 (b) $\bar{M}_n = \bar{M}_w / (1 + p) = 9,250 \text{ g/mol}$
 (c) Average number of structural units in the polymer molecules =
 $\bar{X}_n = \bar{M}_n / M_o = 92.5$
 (d) $\text{Prob}(185) = p^{x-1}(1-p) = 1.463 \times 10^{-3}$

4. (k at 187°C should be taken as $2.74 \times 10^{-2} \text{ kg/mol-min}$)
 $M_o = 127 \text{ g/mol}$



5. (a) From Problem 4, the reaction is second order. Therefore,

$$-\frac{d[\text{COOH}]}{dt} = k_2[\text{COOH}]^2$$

Integration yields:

$$\frac{1}{[\text{COOH}]} - \frac{1}{[\text{COOH}]_o} = k_2 t$$

But,

$$\bar{X}_n = \frac{1}{1-p} = \frac{[\text{COOH}]_o}{[\text{COOH}]}, \text{ and combination yields:}$$

$$\bar{X}_n = k_2[\text{COOH}]_o t + 1$$

Now, we will modify the expression to account for the presence of 0.65 mol% of caproic acid.

Let $r = [\text{NH}_2]_0 / [\text{COOH}]_0 = 1/1.0065 = 0.9822$. Amine and carboxylic acid groups are consumed in equimolar amounts; thus,
 $[\text{COOH}]_0 - [\text{COOH}] = [\text{NH}_2]_0 - [\text{NH}_2]$

and we have,

$$[\text{NH}_2] = (r - 1)[\text{COOH}]_0 + [\text{COOH}]$$

Therefore,

$$-\frac{d[\text{COOH}]}{dt} = k_2[\text{COOH}]\{(r - 1)[\text{COOH}]_0 + [\text{COOH}]\}$$

Separating variables, integrating, and rearranging yields:

$$\int_{[\text{COOH}]_0}^{[\text{COOH}]} \frac{d[\text{COOH}]}{[\text{COOH}]\{(r - 1)[\text{COOH}]_0 + [\text{COOH}]\}} = -k_2 \int_0^t dt$$

$$\ln \frac{(r - 1)[\text{COOH}]_0 + [\text{COOH}]}{r[\text{COOH}]} = (r - 1)[\text{COOH}]_0 k_2 t, \quad r < 1$$

Or, in terms of the conversion, p , of the minority groups (NH_2):

$$\ln \frac{1 - p}{1 - rp} = (r - 1)[\text{COOH}]_0 k_2 t, \quad r < 1$$

(In this particular case, $r = 0.9822$)

- (b) (Assume that this question refers to the case for which caproic acid is absent.) From Problem 4, the value of the second-order rate constant, k_2 , is 2.74×10^{-2} kg/mol-min.

$$t = \frac{\frac{\bar{M}_n - 18}{M_0} - 1}{[\text{COOH}]_0 k_2} = 539 \text{ min}$$

- (c) The average degree of polymerization in (b) above is 49.78, and hence, the conversion is 0.9799.

12,718 g/mol represents a degree of polymerization of 100.

$$W_x = x(1 - p)^2 p^{x-1} = 5.41 \times 10^{-3}$$

Neglecting the weight of water contained in the terminal groups, the total mass of polymer molecules is 419.1 g (3.3 mol of aminocaproic acid repeat units at 127 g/mol each). Thus, $5.41 \times 10^{-3} \times 419.1 \text{ g} = 2.27 \text{ g}$ of polyamide has a molecular weight of 12,718 g/mol.

6. (a) Let $A = 2[\text{COOH}]_0^2 k_3$. The integrated rate expression for an uncatalyzed polyesterification is given as follows:

$$\frac{1}{(1-p)^2} = 1 + At$$

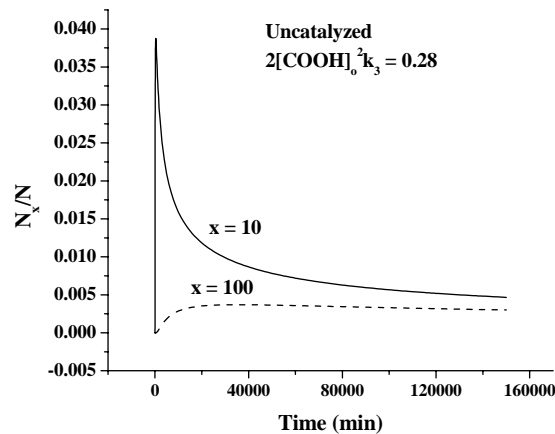
Solve for p:

$$p = 1 - \frac{1}{\sqrt{1+At}} = \frac{\sqrt{1+At} - 1}{\sqrt{1+At}}$$

Combine with equation for Prob (x):

$$\text{Prob}(x) = \frac{N_x}{N} = \frac{(\sqrt{1+At} - 1)^{x-1}}{(\sqrt{1+At})^x}$$

The following is a plot of the mole fraction of polymer with $x = 10$ and $x = 100$ as a function of reaction time, with $A = 0.28$ (this value of A was chosen by setting $[\text{COOH}]_0 = 8 \text{ eq/kg}$ and $k_3 = 0.0022 \text{ kg}^2/\text{eq}^2\text{-min}$):



- (b) Let $B = [\text{COOH}]_0 k_2$. The integrated rate expression for an acid-catalyzed polyesterification is given as follows:

$$\frac{1}{(1-p)} = 1 + Bt$$

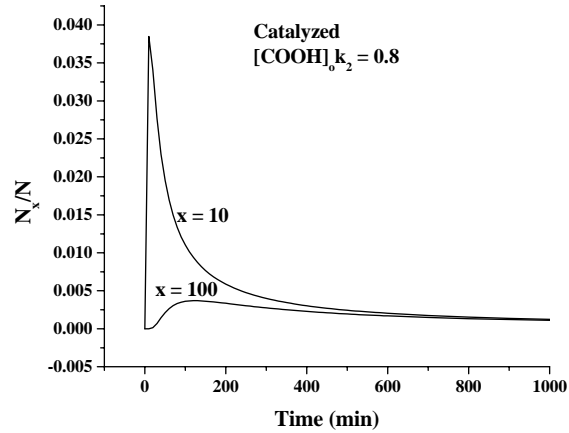
Solve for p:

$$p = 1 - \frac{1}{1+Bt} = \frac{Bt}{1+Bt}$$

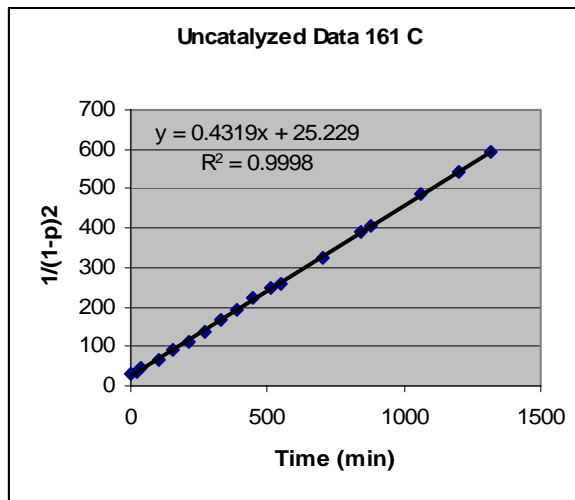
Combine with equation for Prob (x):

$$\text{Prob}(x) = \frac{N_x}{N} = \frac{(Bt)^{x-1}}{(1+Bt)^x}$$

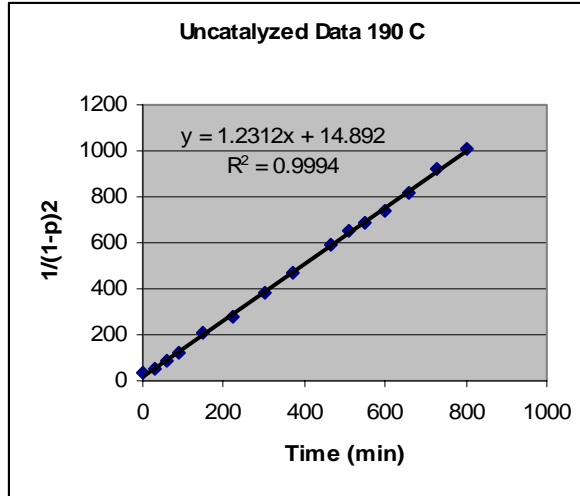
The following is a plot of the mole fraction of polymer with $x = 10$ and $x = 100$ as a function of reaction time, with $B = 0.8$ (this value of B was chosen by setting $[\text{COOH}]_0 = 8 \text{ eq/kg}$ and $k_2 = 0.1 \text{ kg/eq-min}$):



7. (a) The following is a plot of the uncatalyzed data at 161°C . The slope obtained by linear regression is 0.4391 min^{-1} . The slope $= 2[\text{COOH}]_0^2 k_3$; therefore, if $[\text{COOH}]_0 = 6.24 \text{ eq/kg}$, then $k_3 = 5.55 \times 10^{-3} \text{ kg}^2/\text{eq}^2\text{-min}$.



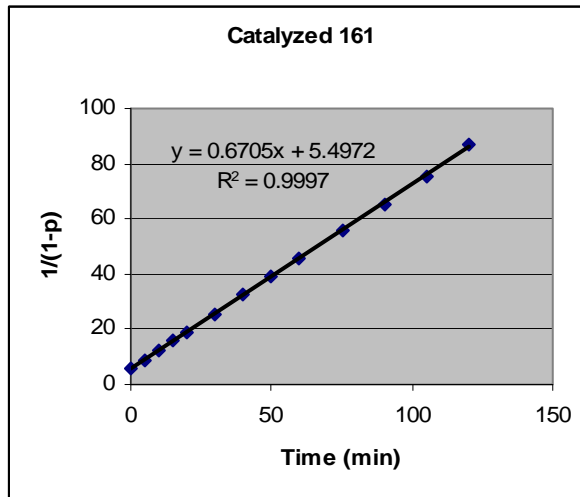
Below is a plot of the uncatalyzed data at 190°C. The slope obtained by linear regression is 1.2312 min^{-1} . The slope = $2[\text{COOH}]_0^2 k_3$; therefore, if $[\text{COOH}]_0 = 6.24 \text{ eq/kg}$, then $k_3 = 1.58 \times 10^{-2} \text{ kg}^2/\text{eq}^2\text{-min}$.



$190^\circ\text{C} = 463\text{K}$; $161^\circ\text{C} = 434\text{K}$

$$E_{act} = -R \ln \frac{k_{3,190}}{k_{3,161}} \left(\frac{1}{463} - \frac{1}{434} \right)^{-1} = 14.4 \frac{\text{kcal}}{\text{mol}}$$

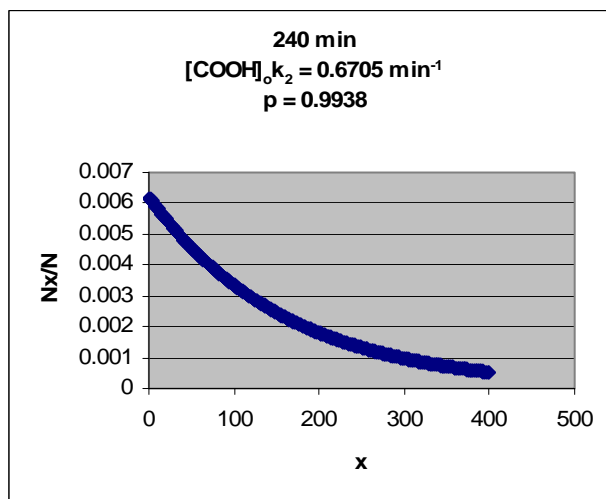
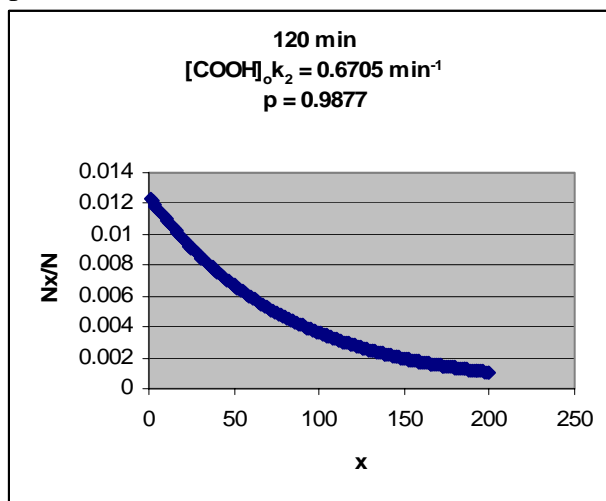
- (b) Below is a plot of the catalyzed data at 161°C. The slope obtained by linear regression is 0.6705 min^{-1} . The slope = $[\text{COOH}]_0 k_2$; therefore, if $[\text{COOH}]_0 = 6.24 \text{ eq/kg}$, then $k_2 = 0.107 \text{ kg/eq-min}$.



8. For the catalyzed polyesterification, $[\text{COOH}]_0 k_2 = 0.6705 \text{ min}^{-1}$. Recall from Problem 6 that for $B = [\text{COOH}]_0 k_2$, the following distribution function holds:

$$\text{Prob}(x) = \frac{N_x}{N} = \frac{(Bt)^{x-1}}{(1+Bt)^x}$$

The following are plots of this function at 120 min ($p=0.9877$) and 240 min ($p=0.9938$):



Let $B = [\text{COOH}]_0 k_2$. Recall, the integrated rate expression for an acid-catalyzed polyesterification is given as follows:

$$\frac{1}{(1-p)} = 1 + Bt$$

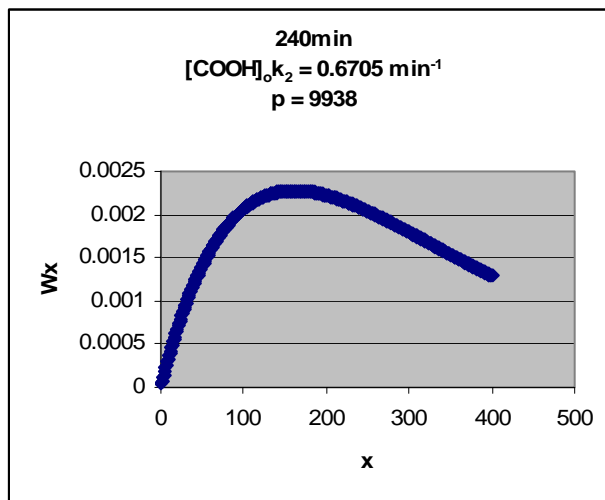
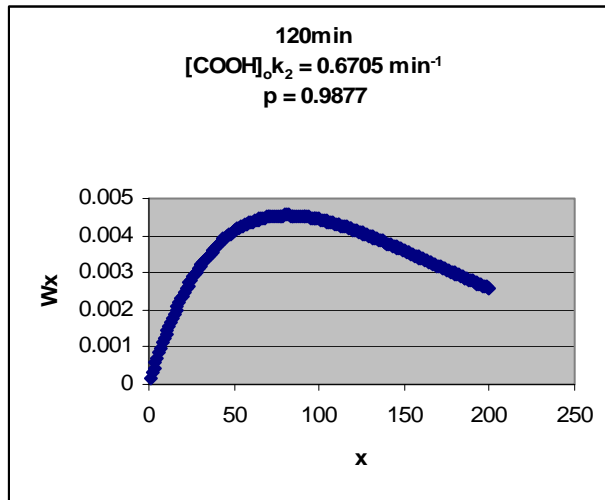
Solve for p :

$$p = 1 - \frac{1}{1+Bt} = \frac{Bt}{1+Bt}$$

Combine with $W_x = x(1-p)^2 p^{x-1}$:

$$W_x = x(1 + Bt)^{-2} \left(\frac{Bt}{1 + Bt} \right)^{x-1}$$

The following are plots of this function at 120 min ($p=0.9877$) and 240 min ($p=0.9938$):



9.
$$r = \frac{N_A}{N_B} = \frac{[\text{Acid}]_0}{[\text{Diol}]_0} = \frac{1 - 0.0085}{1} = 0.9915$$

$$\left(\bar{X}_n \right)_{\max} = \frac{1 + r}{1 - r} = \frac{1.9915}{0.0085} = 234.3$$

For this particular A-A, B-B system, $M_o = 142.2$ g/mol. At full conversion, all molecules will have an odd number of structural units with decanediol units on

both ends; hence, $\bar{X}_n = 2n + 1$, and $n = \frac{r}{1 - r}$.

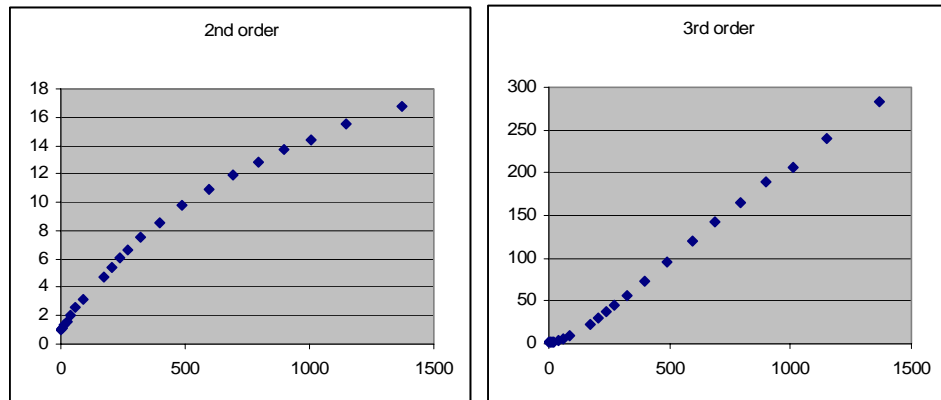
$$\overline{M}_n = (\overline{X}_n - 1)M_o + M_{eg}, \text{ where } M_{eg} \text{ is the molecular weight of the end groups.}$$

In this particular case, this represents one decanediol structural unit plus one water = 174.3 g/mol. Therefore, $\overline{M}_n = 33,348$ g/mol. $\overline{M}_w \cong 2\overline{M}_n = 66,696$ g/mol.

Alternatively, for high degrees of polymerization, \overline{M}_n is very accurately approximated by:

$$\overline{M}_n = \overline{X}_n \cdot M_o = 33,317 \text{ g/mol. And, } \overline{M}_w \cong 2\overline{M}_n = 66,635 \text{ g/mol.}$$

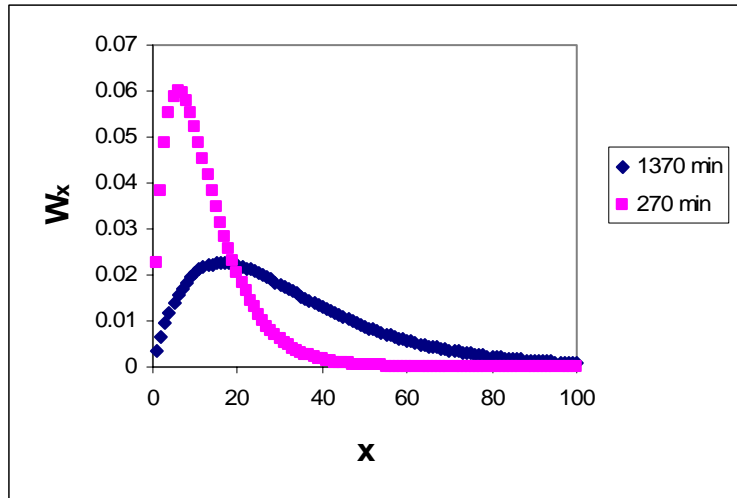
10. (a) The reaction is 3rd order.



$$(b) \quad [COOH]_o = \frac{2 \text{ (eq/mol)}}{(FW_{DEG} + FW_{AA}) \text{ (g/mol)}} 1000 \left(\frac{\text{g}}{\text{kg}} \right) = 7.93 \frac{\text{eq}}{\text{kg}}$$

The slope of the 3rd order plot (from the linear portion above $p = 0.8$) is, by linear regression, equal to 0.22 min^{-1} . Therefore, $k_3 = 1.75 \times 10^{-3} \text{ kg}^2/\text{eq}^2\text{-min}$.

- (c) Below are plots of the function $W_x = x(1-p)^2 p^{x-1}$, at 270 min ($p=0.85$) and 1370 min ($p=0.9405$).



11. Allcock offers no solution for this system. Regarding the Carother's approach, he does not instruct the reader of how to calculate f_{avg} for non-stoichiometrically balanced systems. However, a solution is given in the notes (material taken from Odian).

$$f_{avg} = \frac{2 \sum N_i(A) f_i(A)}{\sum N_i} = \frac{2[(5 \cdot 2)]}{5 + 4 + 1} = \frac{20}{10}$$

$$p_c = \frac{2}{f_{avg}} = 1.0$$

Regarding the statistical approach, Allcock likewise offers no solution. His analysis apparently applies only to systems in which the branching monomer contains the type of group (i.e., A or B) that is in the minority. Again, however, a solution can be found in Odian (p. 110, 4th Ed.).

$$p_c = \frac{1}{[r(f_{w,A} - 1)(f_{w,B} - 1)]^{1/2}} \frac{1}{\left[\frac{10}{11}(2-1)\left(\frac{25}{11}-1\right)\right]^{1/2}} = 0.93$$

Here, $f_{w,A}$ and $f_{w,B}$ are the weight-average functionalities of the A and B containing molecules, given by:

$$f_{w,A} = \frac{\sum f_{A_i}^2 N_{A_i}}{\sum f_{A_i} N_{A_i}} \quad f_{w,B} = \frac{\sum f_{B_i}^2 N_{B_i}}{\sum f_{B_i} N_{B_i}}$$

This approach provides (coincidentally perhaps) the answer given by Allcock.