

1. $k_p = 74 \text{ L/mol-sec}$; $k_t = 3.3 \times 10^6 \text{ L/mol-sec}$; $r_i = 10^{-6} \text{ mol/L-sec}$

(a) $[R] = \left(\frac{r_i}{2k_t} \right)^{1/2} = 3.89 \times 10^{-7} \frac{\text{mol}}{\text{L}}$

(b) $\frac{d[R]}{dt} = r_i - r_t = r_i - 2k_t[R]^2$

Separate variables and expand into partial fractions:

$$\int \frac{d[R]}{r_i - 2k_t[R]^2} = \frac{1}{2\sqrt{2k_t r_i}} \left(\int \frac{\sqrt{2k_t}}{\sqrt{r_i} + [R]\sqrt{2k_t}} d[R] + \int \frac{\sqrt{2k_t}}{\sqrt{r_i} - [R]\sqrt{2k_t}} d[R] \right) = \int dt$$

$$\frac{1}{2\sqrt{2k_t r_i}} \left[\ln(\sqrt{r_i} + [R]\sqrt{2k_t}) - \ln(\sqrt{r_i} - [R]\sqrt{2k_t}) \right] = t$$

$$\ln \frac{\sqrt{r_i} + [R]\sqrt{2k_t}}{\sqrt{r_i} - [R]\sqrt{2k_t}} = 2(2k_t r_i)^{1/2} t$$

Or:

$$[R] = \left(\frac{r_i}{2k_t} \right)^{1/2} \tanh(2k_t r_i)^{1/2} t = \left(\frac{r_i}{2k_t} \right)^{1/2} \frac{e^{(2k_t r_i)^{1/2} t} - e^{-(2k_t r_i)^{1/2} t}}{e^{(2k_t r_i)^{1/2} t} + e^{-(2k_t r_i)^{1/2} t}}$$

Now, find t at $[R] = 0.95 \left(\frac{r_i}{2k_t} \right)^{1/2}$

$$t = \frac{\ln \frac{\sqrt{r_i} + [R]\sqrt{2k_t}}{\sqrt{r_i} - [R]\sqrt{2k_t}}}{2\sqrt{2k_t r_i}} = \frac{\ln \frac{\sqrt{r_i} + 0.95\sqrt{r_i}}{\sqrt{r_i} - 0.95\sqrt{r_i}}}{2\sqrt{2k_t r_i}} = \frac{\ln \frac{1.95}{0.05}}{2\sqrt{2k_t r_i}} = 0.713 \text{ s}$$

(c) Integrate the free-radical polymerization rate equation with respect to monomer ($r_i = \text{constant}$).

$$r_p = \frac{-d[M]}{dt} = \left(\frac{k_p^2}{2k_t} \right)^{1/2} r_i^{1/2} [M] \Rightarrow \ln \frac{[M]_o}{[M]} = \left(\frac{k_p^2}{2k_t} \right)^{1/2} r_i^{1/2} t$$

Find t for which $[M] = 0.8[M]_o$:

$$t = \left(\frac{k_p^2}{2k_t} \right)^{-1/2} r_i^{-1/2} \ln \frac{[M]_o}{[M]} = 7.75 \times 10^3 \text{ s}$$

- (d) Instead of assuming the steady-state concentration from the beginning of the reaction, utilize the expression for $[R]$ as a function of time developed in section (b) above. $[R]_{SS}$ = steady-state radical concentration.

$$\frac{-d[M]}{dt} = k_p \left(\frac{r_i}{2k_t} \right)^{1/2} [M] \tanh(2k_t r_i)^{1/2} t$$

Integrate:

$$-\int \frac{d[M]}{[M]} = k_p [R]_{SS} \int \frac{e^{at} - e^{-at}}{e^{at} + e^{-at}} dt \quad \text{where, } [R]_{SS} = \left(\frac{r_i}{2k_t} \right)^{1/2} \text{ and, } a = (2k_t r_i)^{1/2}$$

$$-\ln[M] \Big|_{[M]_o}^{[M]} = k_p [R]_{SS} \frac{1}{a} \ln(e^{at} + e^{-at}) \Big|_0^t$$

$$\ln \frac{[M]_o}{[M]} = k_p [R]_{SS} \frac{1}{a} \ln \frac{e^{at} + e^{-at}}{2} \Rightarrow \ln \frac{[M]_o}{[M]} = k_p [R]_{SS} (2k_t r_i)^{-1/2} \ln \frac{e^{(2k_t r_i)^{1/2} t} + e^{-(2k_t r_i)^{1/2} t}}{2}$$

This expression takes the following form at long times ($t \geq \frac{10}{\sqrt{2k_t r_i}}$ sec or so):

$$\ln \frac{[M]_o}{[M]} = k_p [R]_{SS} \left(t - \frac{\ln 2}{(2k_t r_i)^{1/2}} \right)$$

According to this equation, the time required to reach 20% conversion is 0.270 s longer than calculated in section (c) above. This amounts to an error of roughly 3×10^{-3} %.

2. (a) Yes. A plot of r_p vs. $[MMA][AIBN]^{1/2}$ is linear. Also, plots of $r_p/[MMA]$ vs. $[AIBN]^{1/2}$ and $r_p/[AIBN]^{1/2}$ vs. $[MMA]$ are linear.

- (b) $k_i (77^\circ\text{C}) = 9.89 \times 10^{-5} \text{ s}^{-1}$; thus, $(2fk_i)^{1/2} = 1.18 \times 10^{-2} (\text{mol/L} \cdot \text{s})^{1/2}$.

The slope of the r_p vs. $[MMA][AIBN]^{1/2}$ plot is $\left(\frac{k_p^2}{2k_t} \right)^{1/2} (2fk_i)^{1/2}$. Therefore:

$$\left(\frac{k_p^2}{2k_t} \right)^{1/2} = \text{slope} \times (2fk_i)^{-1/2} = 0.00139 \frac{\text{L}^{1/2}}{\text{mol}^{1/2} \cdot \text{s}} \times 85.00 \text{ s}^{1/2} = 0.118 \frac{\text{L}^{1/2}}{\text{mol}^{1/2} \cdot \text{s}^{1/2}}$$

3. (a) The data are in accord with eq. 35. Plots of r_p vs. $[MMA]$ are linear at each temperature (at each temperature, the values of $r_p/[MMA]$ are approximately constant).

(b) The slope of a plot of r_p vs. [MMA] (i.e., the average value of r_p /[MMA]) is equal

to $\left(\frac{k_p^2}{2k_t}\right)^{1/2} (2fk_i)^{1/2} [I]^{1/2}$. Therefore,

$$E_p - \frac{1}{2}E_t + \frac{1}{2}E_i = -R \ln \frac{\text{slope}_{50}}{\text{slope}_{70}} \left(\frac{1}{323} - \frac{1}{343}\right)^{-1} = 19.6 \frac{\text{kcal}}{\text{mol}}$$

(c) From Table 12.2, for MMA, $E_p - E_t/2 = 4.9$ kcal/mol. Using the answer from (b) above, E_i for benzoyl peroxide = 29.4 kcal/mol.

(d) $\bar{X}_n (\overline{DP})$ is proportional to [MMA], as predicted by eqs. (39) and (43). Since

$$\bar{X}_n \propto \exp\left[\frac{-(E_p - E_t/2 - E_i/2)}{RT}\right], \text{ and the overall activation energy is negative,}$$

\bar{X}_n goes down as temperature goes up.

$$4. \quad W_n = X_n \frac{n}{\bar{X}_n}$$

W_n is the weight fraction of polymer chains containing exactly n repeat units.

X_n is the mole fraction of polymer chains containing exactly n repeat units.

\bar{X}_n is the average degree of polymerization of the polymer.

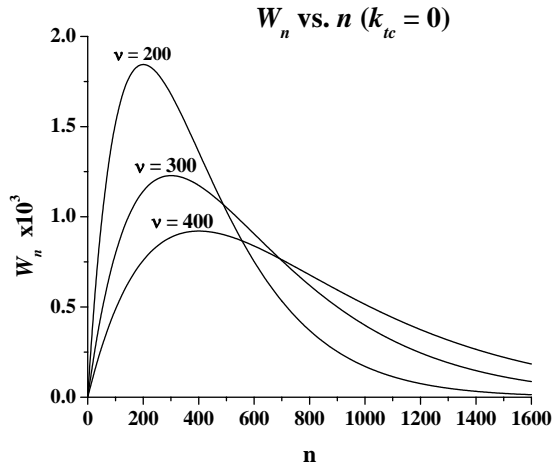
$$\text{And, } \bar{X}_n = 2\nu \frac{k_{tc} + k_{td}}{k_{tc} + 2k_{td}} \text{ (eq. (43)).}$$

Combination of eq. (66) and (43) with the equation at the top of this problem yields:

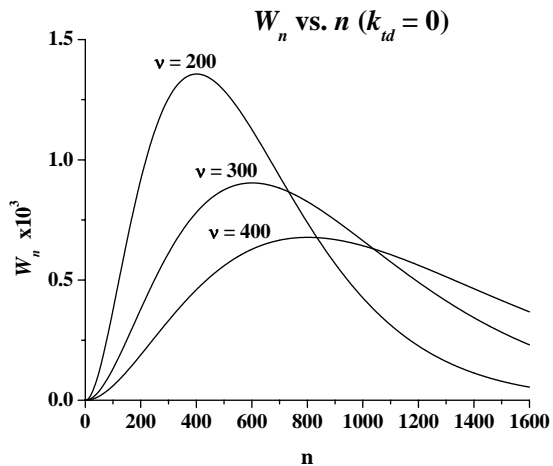
$$W_n = \frac{1}{\nu} \left(1 + \frac{1}{\nu}\right)^{-n} \frac{(n-1)/\nu + 2(k_{td}/k_{tc})}{1 + 2(k_{td}/k_{tc})} \left(\frac{n}{2\nu}\right) \frac{1 + 2(k_{td}/k_{tc})}{1 + (k_{td}/k_{tc})}$$

$$W_n = \frac{n}{2\nu^2} \left(1 + \frac{1}{\nu}\right)^{-n} \frac{(n-1)/\nu + 2(k_{td}/k_{tc})}{1 + (k_{td}/k_{tc})}$$

5. (a) For $k_{tc} = 0$, $W_n = \frac{n}{v^2} \left(1 + \frac{1}{v}\right)^{-n}$



(b) For $k_{td} = 0$, $W_n = \frac{n(n-1)}{2v^3} \left(1 + \frac{1}{v}\right)^{-n}$



6. Apply steady-state approximation to radicals of degree of polymerization, n :

$$\frac{d[R_n]}{dt} = k_p[M][R_{n-1}] - k_p[M][R_n] - 2k_t[R_n][R] - (k_M[M] + k_S[S] + k_Y[Y])[R_n] = 0$$

Introduce, $\gamma = C_M + C_S \frac{[S]}{[M]} + C_Y \frac{[Y]}{[M]}$, to yield:

$$\frac{d[R_n]}{dt} = k_p[M][R_{n-1}] - k_p[M][R_n] - 2k_t[R_n][R] - k_p[M][R_n]\gamma = 0 \quad 6-1$$

Rearrange:

$$\frac{[R_n]}{[R_{n-1}]} = \left(\frac{k_p[M] + 2k_t[R] + k_p[M]\gamma}{k_p[M]} \right)^{-1} = \left(1 + \frac{1}{\nu} + \gamma \right)^{-1} \quad 6-2$$

To obtain $[R_n]/[R_1]$:

$$\frac{[R_n]}{[R_1]} = \left(\frac{[R_n]}{[R_{n-1}]} \right) \left(\frac{[R_{n-1}]}{[R_{n-2}]} \right) \left(\frac{[R_{n-2}]}{[R_{n-3}]} \right) \dots \frac{[R_2]}{[R_1]} = \left(1 + \frac{1}{\nu} + \gamma \right)^{1-n} \quad 6-3$$

f_n is defined as the fraction of propagating radicals that has a degree of polymerization n . Combine with 6-3:

$$f_n = \frac{[R_n]}{[R]} = \frac{[R_1]}{[R]} \left(1 + \frac{1}{\nu} + \gamma \right)^{1-n} \quad 6-4$$

Now, apply the steady-state approximation to $[R]$ and $[R_1]$:

$$\frac{d[R]}{dt} = r_i - 2k_t[R]^2 = 0 \quad 6-5$$

$$\frac{d[R_1]}{dt} = r - k_p[M][R_1] - 2k_t[R_1][R] - k_p[M][R_1]\gamma + k_p[M][R]\gamma = 0 \quad 6-6$$

The last term in 6-6 accounts for the fact that chain transfer produces (after reaction of the primary radical with monomer) a new radical of degree of polymerization of 1. Combine 6-5 and 6-6:

$$\frac{[R_1]}{[R]} = \frac{2k_t[R] + k_p[M]\gamma}{k_p[M] + 2k_t[R] + k_p[M]\gamma} = \left(\frac{1 + \frac{1}{\nu} + \gamma}{\frac{1}{\nu} + \gamma} \right)^{-1} \quad 6-7$$

Combine 6-4 and 6-7 to yield the distribution function.

$$f_n = \frac{[R_n]}{[R]} \left(\frac{1}{\nu} + \gamma \right) \left(1 + \frac{1}{\nu} + \gamma \right)^{-n} \quad 6-8$$

The mole fraction of polymer with degree of polymerization of n is represented as X_n and is defined by the rate of formation of polymer with degree of polymerization of n , P_n , divided the rate of formation of polymer of all degrees of polymerization, P .

$$X_n = \frac{d[P_n]/dt}{d[P]/dt} \quad 6-9$$

The rate of formation of P is:

$$\frac{d[P]}{dt} = (k_{tc} + 2k_{td})[R]^2 + k_p[M][R]\gamma = [(k_{tc} + 2k_{td}) + 2v\gamma(k_{tc} + k_{td})][R]^2 \quad 6-10$$

For even n ,

$$\frac{d[P_n]}{dt} = k_{tmc}[R_{n/2}][R_{n/2}] + \frac{1}{2} \sum_{\substack{m=1 \\ m \neq n/2}}^{n-1} k_{tmc}[R_m][R_{n-m}] + 2k_{td}[R_n][R] + k_p[M][R_n]\gamma \quad 6-11$$

The rate constant for termination of unlike radicals, k_{tmm} , is twice that of like radicals, k_{tmm} (i.e., $k_{tmm} = 2k_{tmm} = 2k_t$). (In the absence of an “ nn ” or “ nm ” subscript, k_t is understood to be the rate constant for termination of like radicals.)

$$\frac{d[P_n]}{dt} = k_{tc} \sum_{m=1}^{n-1} [R_m][R_{n-m}](1)^m + 2k_{td}[R_n][R] + k_p[M][R_n]\gamma \quad 6-12$$

6-12 also holds for odd n . Substitute 6-8.

$$\frac{d[P_n]}{dt} = \left[k_{tc} \left(\frac{1}{v} + \gamma \right)^2 \left(1 + \frac{1}{v} + \gamma \right)^{-n-1} \sum_{m=1}^{n-1} (1)^m + 2k_{td} \left(\frac{1}{v} + \gamma \right) \left(1 + \frac{1}{v} + \gamma \right)^{-n} + \frac{k_p[M]}{[R]} \gamma \left(\frac{1}{v} + \gamma \right) \left(1 + \frac{1}{v} + \gamma \right)^{-n} \right] [R]^2$$

Combine terms.

$$\frac{d[P_n]}{dt} = \left(\frac{1}{v} + \gamma \right) \left(1 + \frac{1}{v} + \gamma \right)^{-n} \left\{ \left[\left(\frac{1}{v} + \gamma \right) (n-1) + 2v\gamma \right] k_{tc} + (2 + 2v\gamma) k_{td} \right\} [R]^2$$

Divide by 6-10 and introduce $\alpha = k_{td}/k_{tc}$.

$$X_n = \frac{\left(\frac{1}{v} + \gamma \right) \left(1 + \frac{1}{v} + \gamma \right)^{-n} \left[\left(\frac{1}{v} + \gamma \right) (n-1) + 2v\gamma + (2 + 2v\gamma)\alpha \right]}{1 + 2v\gamma + (2 + 2v\gamma)\alpha}$$

Rearrange.

$$X_n = \left(\frac{1 + v\gamma}{v} \right) \left(1 + \frac{1}{v} + \gamma \right)^{-n} \left[\frac{(n-1) \left(\frac{1 + v\gamma}{v} \right) + 2v\gamma \left(1 + \alpha + \frac{\alpha}{v\gamma} \right)}{1 + 2v\gamma \left(1 + \alpha + \frac{\alpha}{v\gamma} \right)} \right]$$

The following obtains for $k_{td} = 0$ (i.e., $\alpha = 0$):

$$X_n = \left(\frac{1 + v\gamma}{v} \right) \left(1 + \frac{1}{v} + \gamma \right)^{-n} \frac{(n-1) \left(\frac{1 + v\gamma}{v} \right) + 2v\gamma}{1 + 2v\gamma}$$

7. The following obtains for $k_{tc} = 0$:

$$X_n = \left(\frac{1 + \nu\gamma}{\nu} \right) \left(1 + \frac{1}{\nu} + \gamma \right)^{-n}$$

9. $[M] = 4 \text{ M}$; $[I] = 0.05 \text{ M}$; $T = 60^\circ\text{C}$ (333K); $k_i = 1.20 \times 10^{-6} \text{ s}^{-1}$; $f = 0.75$; $k_{tc} = 0$.

$$r_i^{1/2} = (2fk_i)^{1/2} [I]^{1/2} = 3.0 \times 10^{-4} \left(\frac{\text{M}}{\text{s}} \right)^{1/2}$$

From the chapter:

$$k_p = 1.0 \times 10^3 \text{ M}^{-1}\text{s}^{-1} \quad \text{and} \quad k_t = 3.2 \times 10^7 \text{ M}^{-1}\text{s}^{-1};$$

$$\text{therefore,} \quad \left(\frac{k_p^2}{2k_t} \right)^{1/2} = 0.125 \left(\frac{\text{L}}{\text{mol} \cdot \text{s}} \right)^{1/2}$$

$$(a) \quad r_p = \left(\frac{k_p^2}{2k_t} \right)^{1/2} (2fk_i)^{1/2} [I]^{1/2} [M] = 1.5 \times 10^{-4} \left(\frac{\text{M}}{\text{s}} \right)$$

$$(b) \quad \nu = \left(\frac{k_p^2}{2k_t} \right)^{1/2} \frac{[M]}{r_i^{1/2}} = 1.67 \times 10^3$$

(c) C_M (vinyl acetate at 60°C) = 2.5×10^{-4}

C_S (vinyl acetate in benzene) = 2.2×10^{-4}

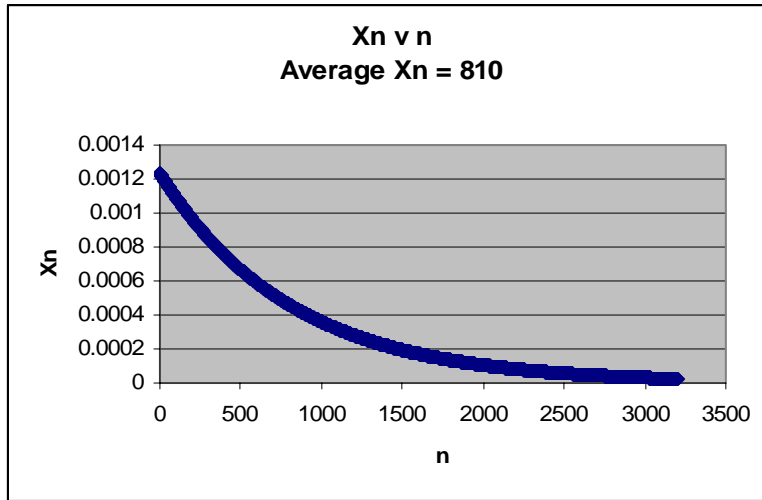
From the densities, and assuming additivity of volumes, $[\text{benzene}] = 7.0 \text{ M}$

For $k_{tc} = 0$,

$$\left(\bar{X}_n \right)^{-1} = C_M + C_S \frac{[S]}{[M]} + \frac{1}{\nu} = 1.24 \times 10^{-3}$$

$$\bar{X}_n = 8.10 \times 10^2$$

$$(d) \quad X_n = \left(\frac{1 + \nu\gamma}{\nu} \right) \left(1 + \frac{1}{\nu} + \gamma \right)^{-n}$$



$$(e) \quad \bar{\tau}_s = \frac{k_p}{2k_t} \left(\frac{[M]}{r_p} \right) = 0.42 \text{ s}$$

$$(f) \quad \bar{\tau}_{s,15} = \frac{\bar{\tau}_s}{\nu} = 2.5 \times 10^{-4} \text{ s}$$

10. $[M] = 8.6 \text{ M}$; $[CCl_4] = 0.1 \text{ M}$; $T = 0^\circ\text{C} (273\text{K})$; $\nu = 1000$.
 From the activation data in Table 12.3,
 $C_{CCl_4,273K} = 1.75 \times 10^{-3}$ and $C_{M,273K} = 4.4 \times 10^{-6}$.

From the activation data in Table 12.2, $\left(\frac{k_p^2}{2k_t} \right)_{273K}^{1/2} = 3.28 \times 10^{-3} \left(\frac{\text{L}}{\text{mol} \cdot \text{s}} \right)^{1/2}$

$$(a) \quad r_{i,273K} = \left(\frac{k_p^2}{2k_t} \right) \left(\frac{[M]}{\nu} \right)^2 = 8.0 \times 10^{-10} \frac{\text{M}}{\text{s}}$$

- (b) From the data in Problem 6, Chap. 3, activation of the rate constant ratio k_{tc}/k_{td} is given by $\ln(k_{tc}/k_{td}) = -7.77 + 5.8 \text{ kcal/mol}/RT$ (i.e., $\ln(A_{tc}/A_{td}) = -7.77$, $E_{tc} - E_{td} = -5.8 \text{ kcal/mol}$). Therefore, at 273K, $k_{tc}/k_{td} = 20$.

$$\left(\bar{X}_n \right)^{-1} = C_{CCl_4} \frac{[CCl_4]}{[M]} + C_M + \frac{k_{tc} + 2k_{td}}{2\nu(k_{tc} + k_{td})} = 5.5 \times 10^{-4}$$

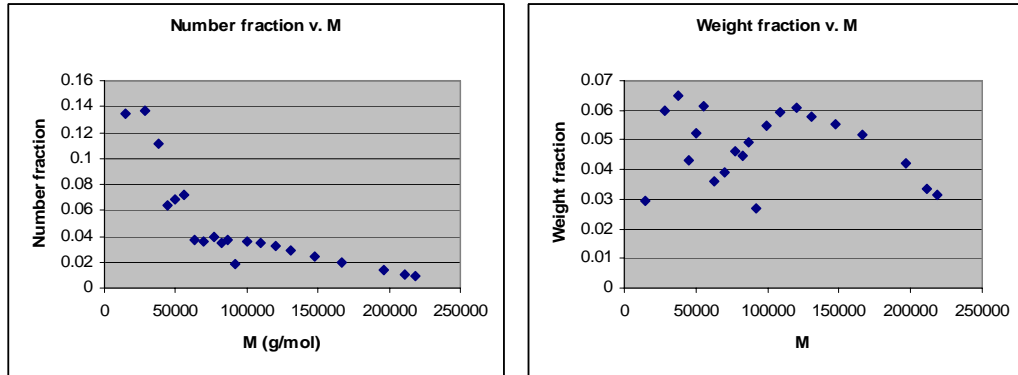
$$\bar{X}_n = 1.8 \times 10^3$$

- (c) Assuming that r_i stays the same (i.e., the rate of photochemical initiation is temperature independent),

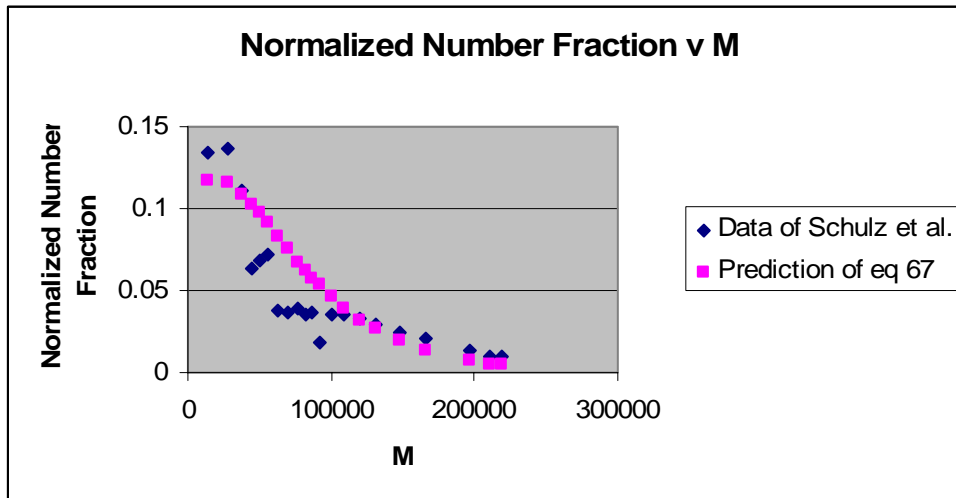
$$v_{373K} = v_{273K} \left(\frac{k_p^2}{2k_t} \right)_{373}^{1/2} \left(\frac{k_p^2}{2k_t} \right)_{273}^{-1/2} = 2.6 \times 10^4$$

At 373K, $k_{tc}/k_{td} = 1.12$, $C_M = 2.15 \times 10^{-4}$, $C_{CCl_4} = 2.07 \times 10^{-2}$. Therefore,
 $\bar{X}_n = 2.07 \times 10^3$

11. Assume $k_{td}/k_{tc} = 0.24$. From the data, $\bar{X}_n = 626$ and, $\nu = 374$.



The following chart plots the experimental number distribution data above, against the theoretical prediction of eq 66 (plotted as X_n v. M). The agreement between data and theory is fair.



12. $M_1 = \text{vinyl acetate}; M_2 = \text{vinyl chloride}$
 $[M_1] = 3.5 \text{ M}; [M_2] = 1.5 \text{ M}$
 $r_1 = 0.23; r_2 = 1.68$

(a)
$$\gamma = \frac{f_1}{f_2} = \frac{1 + r_1([M_1]/[M_2])}{1 + r_2([M_2]/[M_1])} = 0.893$$

$f_1 = 0.47; f_2 = 0.53$

$$(b) \quad \bar{m}_{M_1} = 1 + r_1 \frac{[M_1]}{[M_2]} = 1.54$$

$$\bar{m}_{M_2} = 1 + r_2 \frac{[M_2]}{[M_1]} = 1.72$$

$$(c) \quad R = \frac{200}{m_{M_1} + m_{M_2}} = 61.4$$

$$(d) \quad P_{M_1}(8) = P_{11}^{8-1} P_{12} = 4.1 \times 10^{-4}$$

13. (a)

acrylonitrile (1) – butadiene (2)

$$r_1 = \frac{Q_1}{Q_2} \exp[-e_1(e_1 - e_2)] = 0.017$$

$$r_2 = \frac{Q_2}{Q_1} \exp[-e_2(e_2 - e_1)] = 0.375$$

$$(b) \quad r_1 \text{ (methyl acrylate)} = 7.51$$

$$r_2 \text{ (vinyl chloride)} = 0.113$$

$$(c) \quad r_1 \text{ (methyl vinyl ketone)} = 0.207$$

$$r_2 \text{ (p-methoxystyrene)} = 0.182$$

$$(d) \quad r_1 \text{ (styrene)} = 0.942$$

$$r_2 \text{ (p-methoxystyrene)} = 0.964$$